

Worldwide Pollution Control Association

Duke Energy Seminar
September 3 – 5, 2008
Concord, NC



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Utility Experience with SCR SO₃ Effects

Duke Energy – Belews Creek Steam Station



September 4, 2008

2008 WPCA / Duke Energy Seminar

Introduction

- Understanding SO₃ & ABS
- Determining T_{min}
- Monitoring & Controlling T_{min}
- SCR SO₃ Impacts
- SCR Low-Temp Operation
- APH SO₃ Impacts



Understanding SO_3 & ABS

Sulfur Trioxide (SO_3)

- $> 320^\circ\text{F}$ Gas Phase SO_3
- $\sim 280^\circ\text{F}$ to 320°F H_2SO_4 Vapor Phase
- $< 280^\circ\text{F}$ H_2SO_4 Liquid Phase – Acid Dew Point

ABS - Ammonium Bisulfate – (NH_4HSO_4)

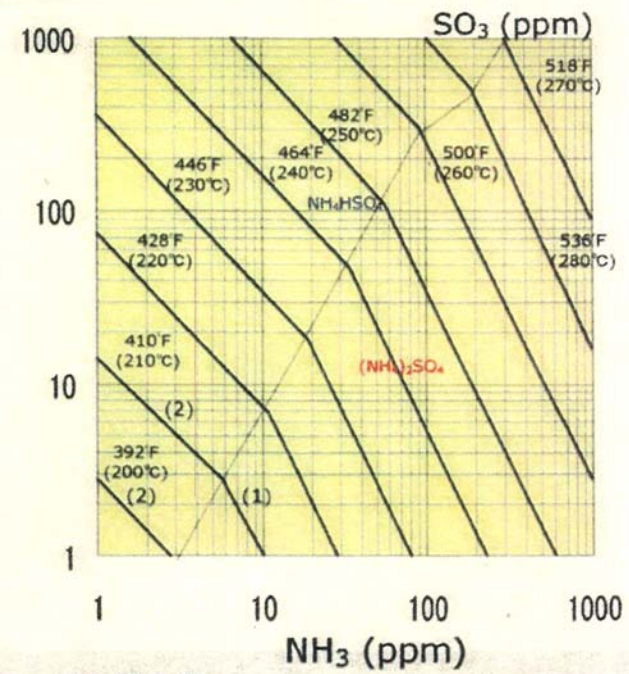
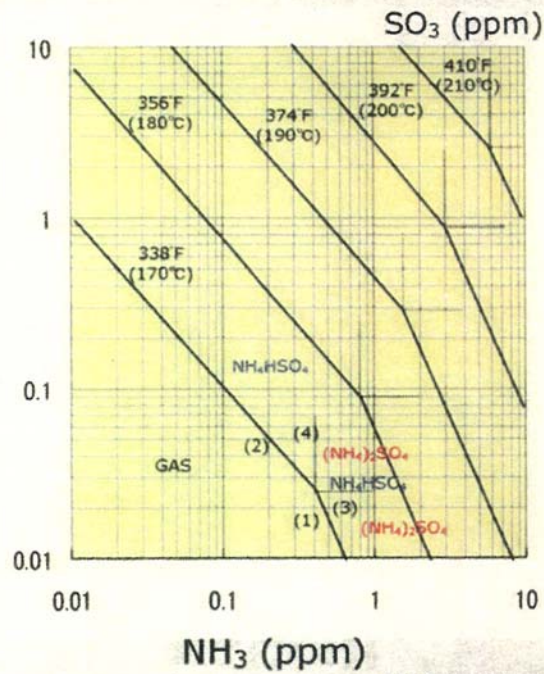
- $> 625^\circ\text{F}$ Dissociates
- $\sim 625^\circ\text{F}$ to 420°F Vapor Phase
- $< 420^\circ\text{F}$ Liquid/Sticky Solid Phase – ABS Dew Point



Determining T_{min} - Theoretical

LT-2

SCR Design & Operation Requirement - Minimum Operating Temperature (Dew Point)

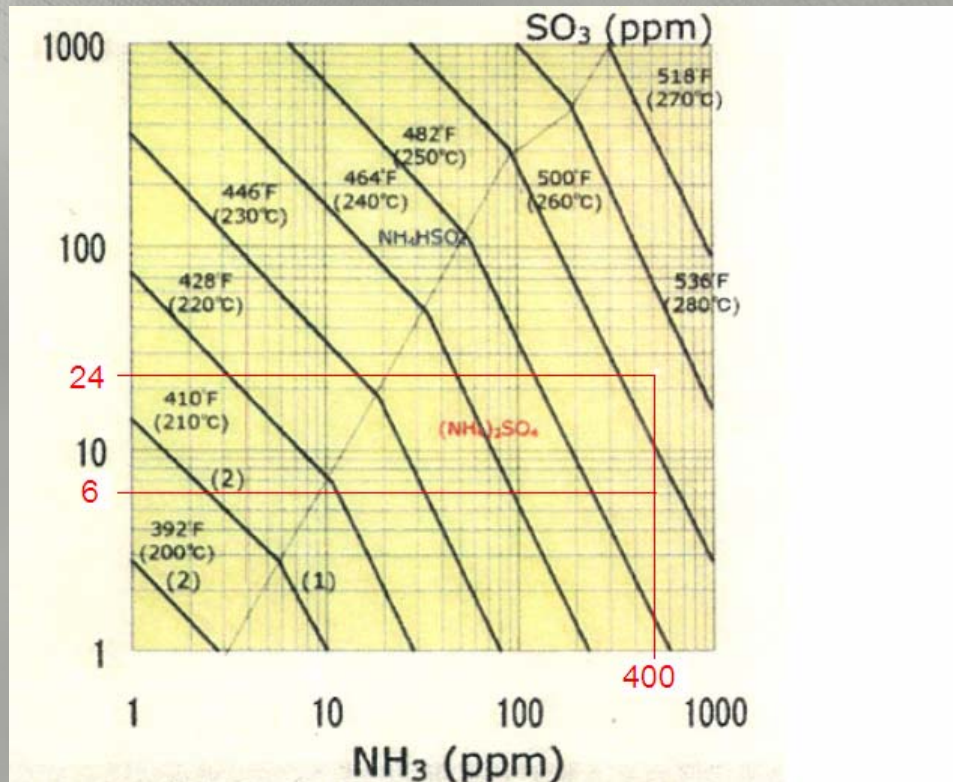


- (1) $2\text{NH}_3 + \text{SO}_3 + \text{H}_2\text{O} \rightleftharpoons (\text{NH}_4)_2\text{SO}_4$
- (2) $\text{NH}_3 + \text{SO}_3 + \text{H}_2\text{O} \rightleftharpoons \text{NH}_4\text{HSO}_4(\text{l})$
- (3) $(\text{NH}_4)_2\text{SO}_4 + \text{SO}_3 + \text{H}_2\text{O} \rightleftharpoons 2\text{NH}_4\text{HSO}_4(\text{l})$
- (4) $\text{NH}_4\text{HSO}_4 + \text{NH}_3 \rightleftharpoons (\text{NH}_4)_2\text{SO}_4$

[ATM, H_2O : 10%]



Determining T_{\min} – Specific

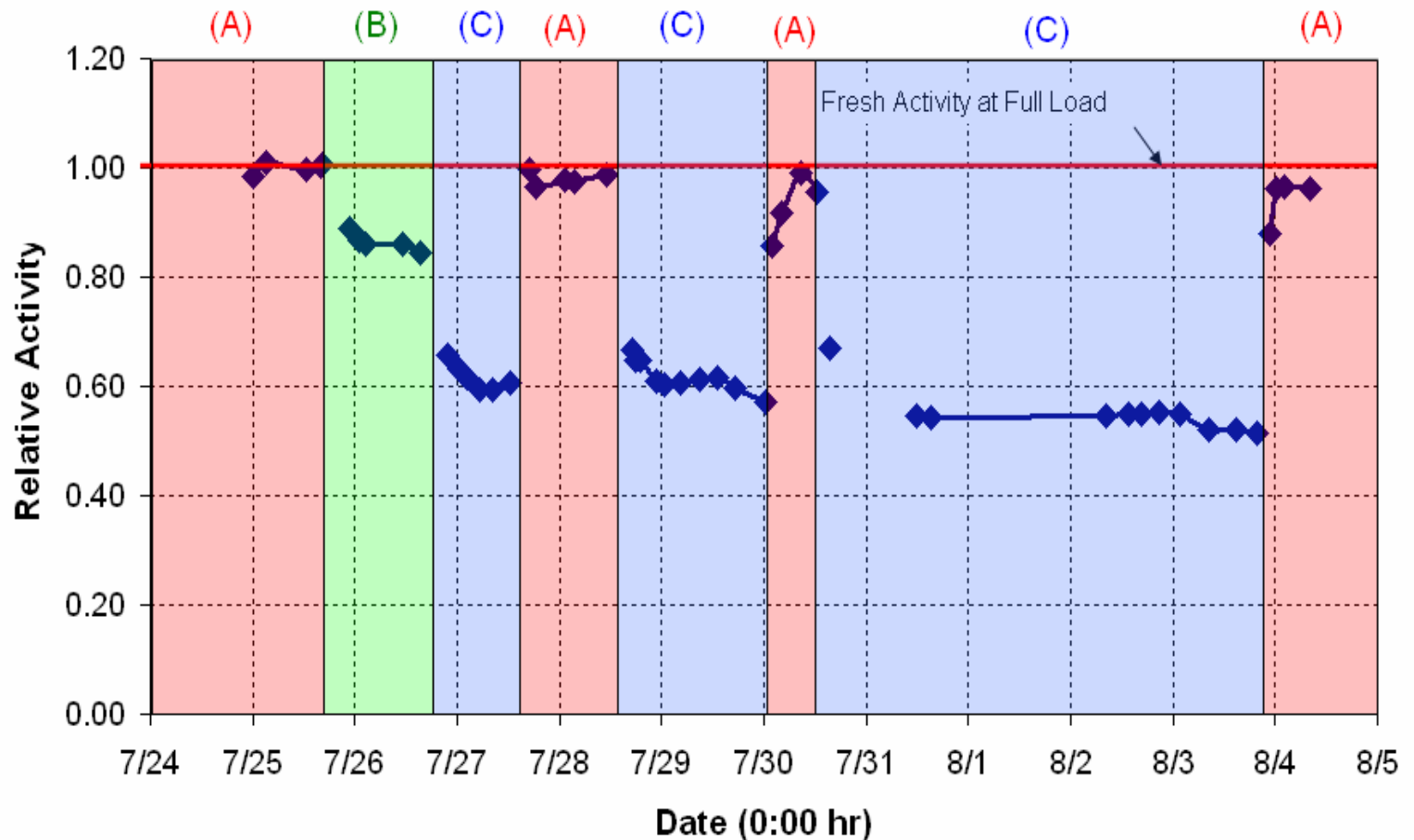


- NH_3 Concentration = Inlet NO_x Concentration
- Furnace $\text{SO}_2 \rightarrow \text{SO}_3$ Conversion = 1%
- Select Dew Point Temperature from Chart
- Add +60°F for Capillary Negative Pressure
- Add +10°F for Temperature Mal-distribution



SCR Low-Temperature Operation

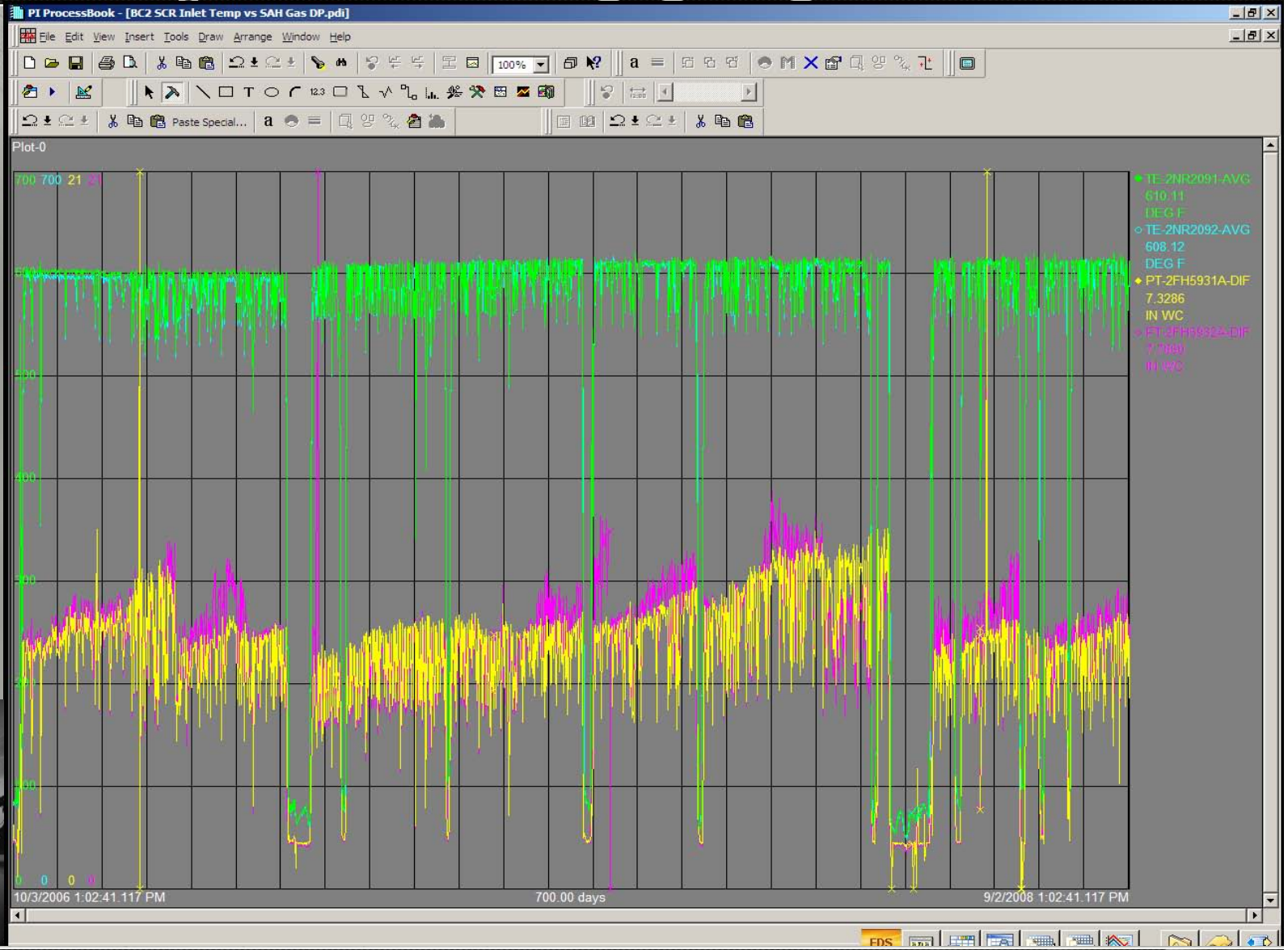
Cormetech Pilot Tests - Low Temperature Operation



(A) Operation at full load temperature. (B) Operation at 25 °F below minimum injection temperature.
(C) Operation at 65 °F below minimum injection temperature (MIT).



APH SO_3 /ABS Pluggage



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Conclusions

- SCR T_{\min} is Unit Specific
- Correct Determination of T_{\min} is Critical
- Low-Temperature Operation Requires Recovery @ $>$ ABS Dew Point Temp
- No Permanent Deactivation of Catalyst after Recovery
- Extended Period Low-Temperature Operation Requires Slower Ramp-up to Avoid Overwhelming SCR and SAH.
- Recovery @ Lower Temperature is Possible with Less or No NH_3 Injection

