

# Reinhold Environmental Ltd.

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2007 NOx Round Table & Expo  
Presentation

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# 2007 NOx Round Table & Expo

## ***FUEL IMPACTS ON CATALYST***

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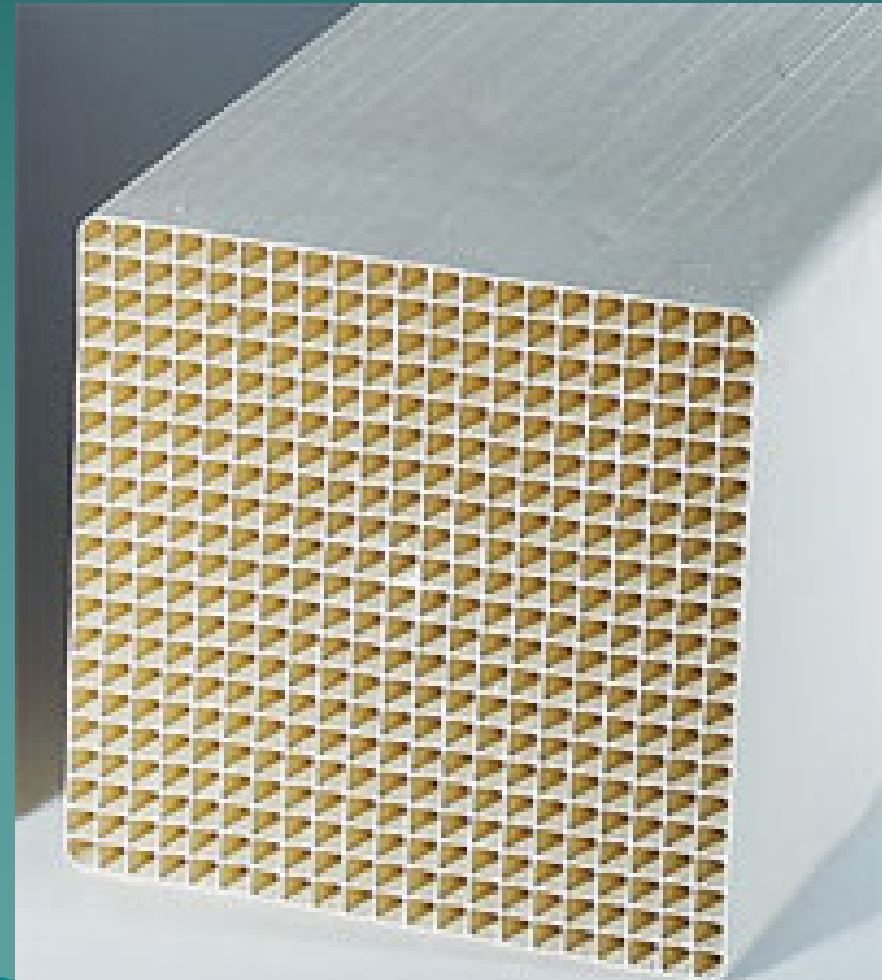
# Key SCR Design Parameters

- Required NO<sub>x</sub> Removal
- SO<sub>2</sub> to SO<sub>3</sub> Conversion Limit
- Ammonia Slip Specification
- Operating Temperature
- Fuel Type

# Catalyst Design

- Geometric and Internal Surface Area
- Support Materials:  $\text{TiO}_2$
- Catalytic Activity: V, W, Mo

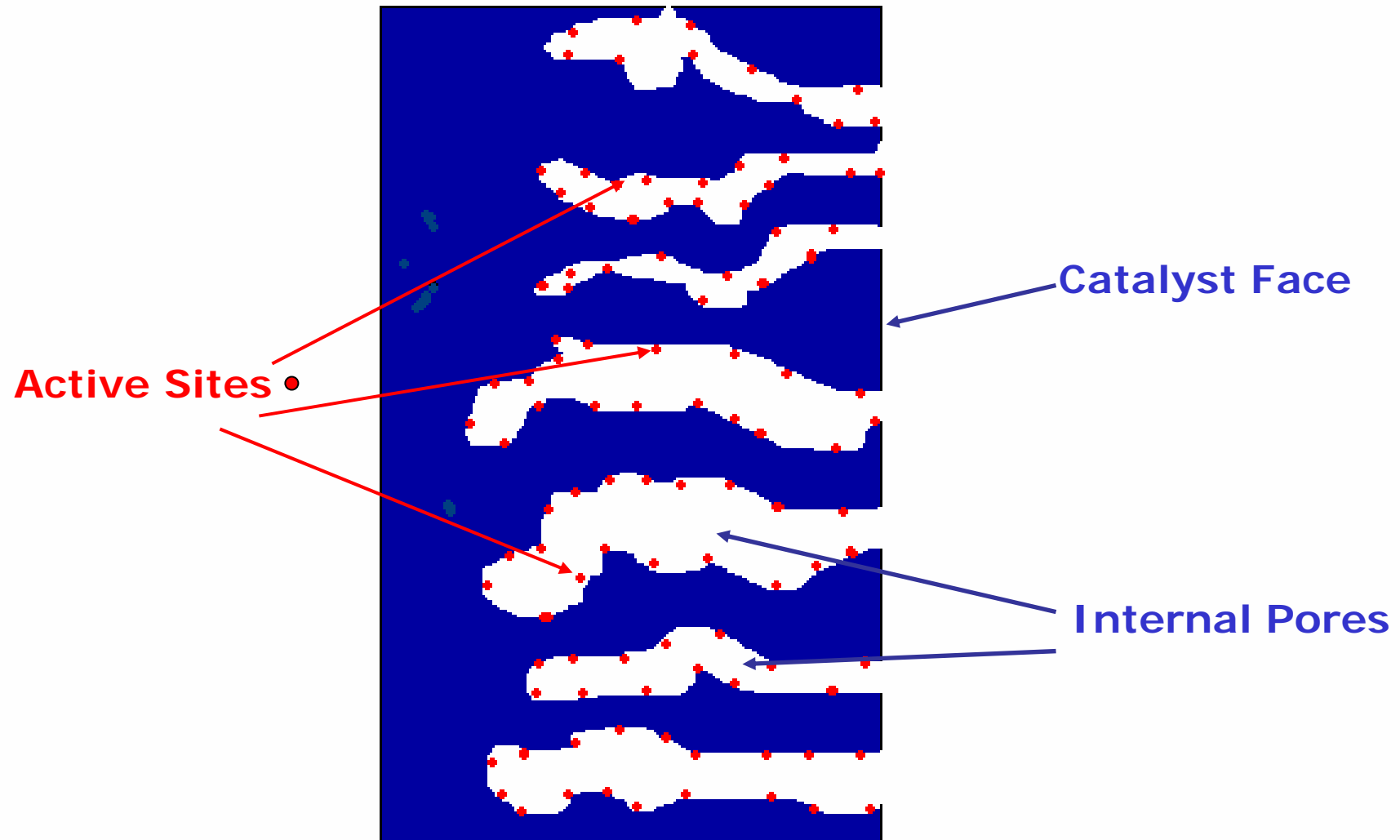
Honeycomb Catalyst



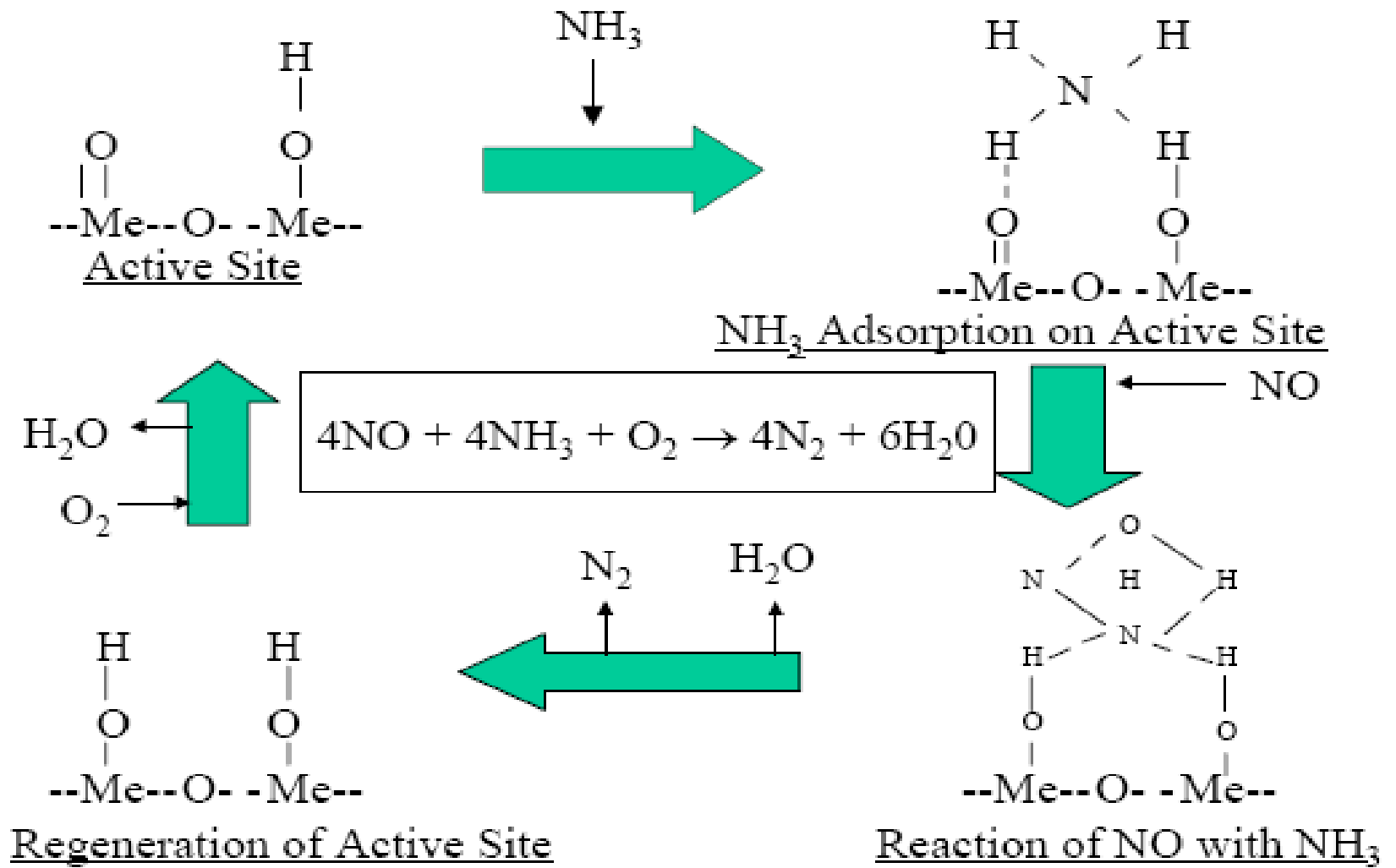
# Plate Catalyst



# Catalyst Design



# Reaction Mechanism



# General Fuel Types

- Natural gas, process gas
- Fuel Oils – low to high sulfur refined petroleum
- Residual refinery products – distillate bottoms
- Refinery Solids – Petroleum Coke
- Coal – bituminous, PRB, lignite, anthracite

# Natural Gas

- Easiest Fuel for SCR Applications
- No Particulate, No Sulfur
- No sootblowing !
- No SO<sub>2</sub> Conv. Limits !
- High activity, small pitch, horizontal and in-duct arrangements
- Long guarantee life
- Slip a function of regulations

# Process Gas

- Often very similar to natural gas
- May contain sulfur, fine particulate
- May have poisons – silica, sodium, potassium, other upstream catalysts
- Unknown/trace components can be problematic
- Highly site specific
- May have little industry experience

# Low-Sulfur Fuel Oil

- Similar to natural gas if high-grade oil is used
- $\text{SO}_2$  conversion can be relaxed if low-sulfur oil is used exclusively
- Sootblowing may not be required
- Horizontal and vertical applications
  - little or no HRSG or APH modifications needed
- Long catalyst lives, small pitch, high activity – slip can be relatively high

# Medium to High-Sulfur Fuel Oil

- Significant sulfur will limit allowable  $\text{SO}_2$  conversion
- Sootblowers are generally required, often preferred over sonic horns
- Horizontal configuration possible with low particulate
- Vanadium in fuel may cause increase in  $\text{SO}_2$  conversion over time
- Significant ABS corrosion may occur
- Possible acid plumes depending on  $\text{SO}_2$  conversion rate and sulfur level

# Refinery Residuals



# Refinery Residuals

- Distillate bottoms, heavy oils
- Typically high sulfur, high particulate, high contaminants; vanadium and others
- May need sootblowing/ vertical configuration
- Strong limits on  $\text{SO}_2$  conversion or mitigation of conversion assoc. with vanadium deposition
- Strong potential for ABS formation
- Stringent limits on ammonia slip
- Highly Fuel Specific

# Pet Coke



# Pet Coke

- High sulfur, high particulate, high contaminants - vanadium
- Sootblowers or sonic horns required, vertical configuration preferred
- Strong limits on SO<sub>2</sub> conversion and mitigation of impacts of vanadium deposition
- Strong impact on downstream equipment due to ABS, sulfuric acid
- Ammonia slip typically low, similar to coal
- Large catalyst pitch

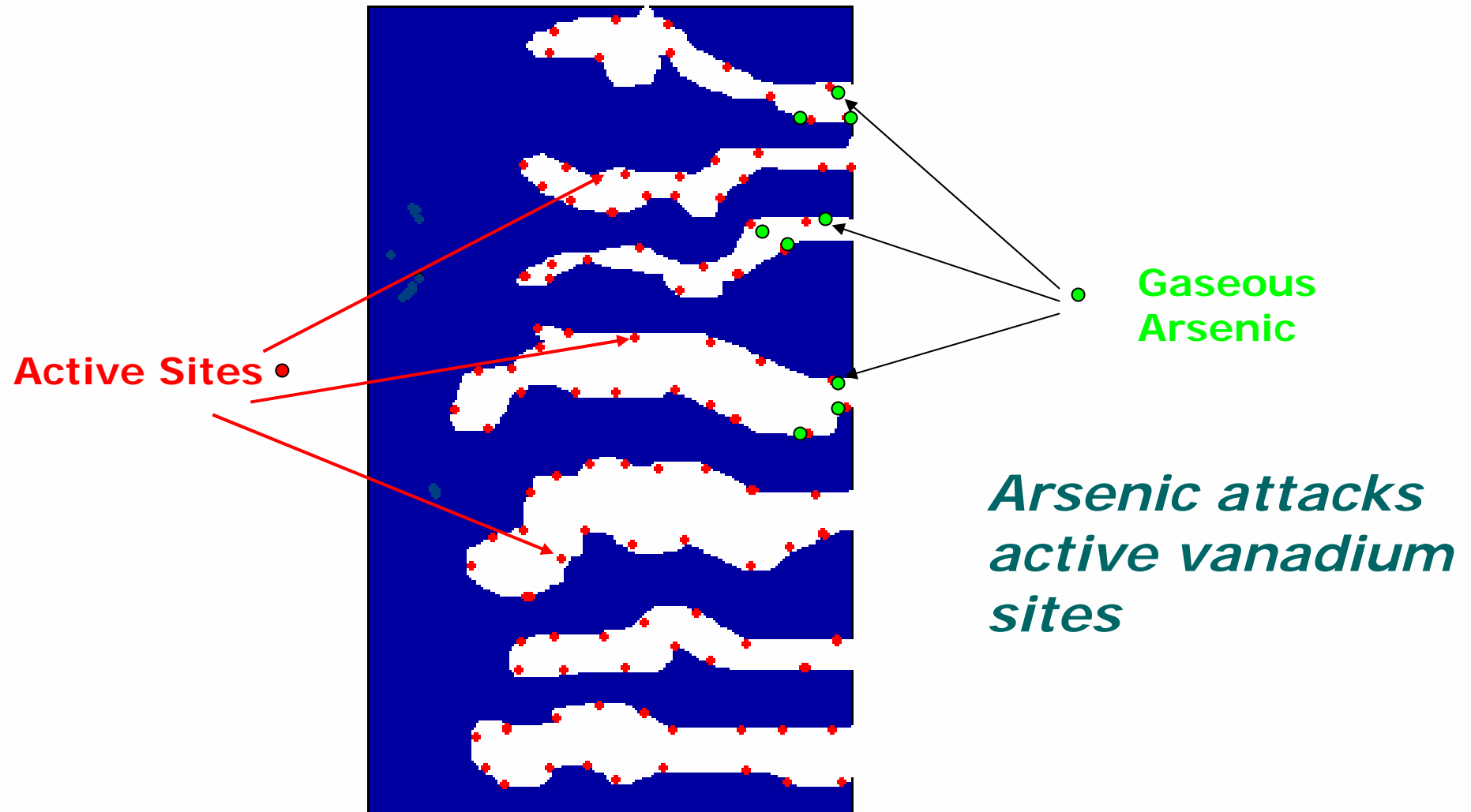
# Bituminous Coal



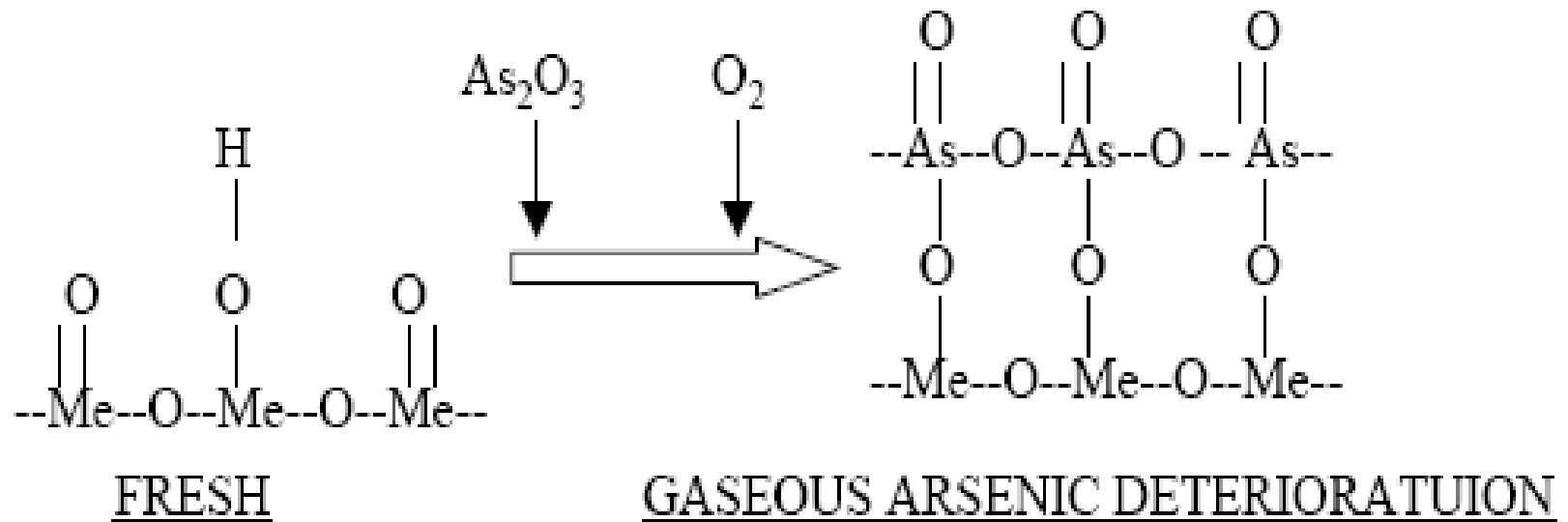
# Bituminous Coal

- Extensive industry experience
- **Poisoned by Arsenic**
- Medium to high sulfur levels, variable ash loading
- Sootblowing required
- Strong limits on SO<sub>2</sub> conversion
- Strong impact on downstream equipment due to ABS, sulfuric acid – APH mods. common
- Ammonia slip typically < 2 ppm
- Life Strongly impacted by calcium and arsenic levels

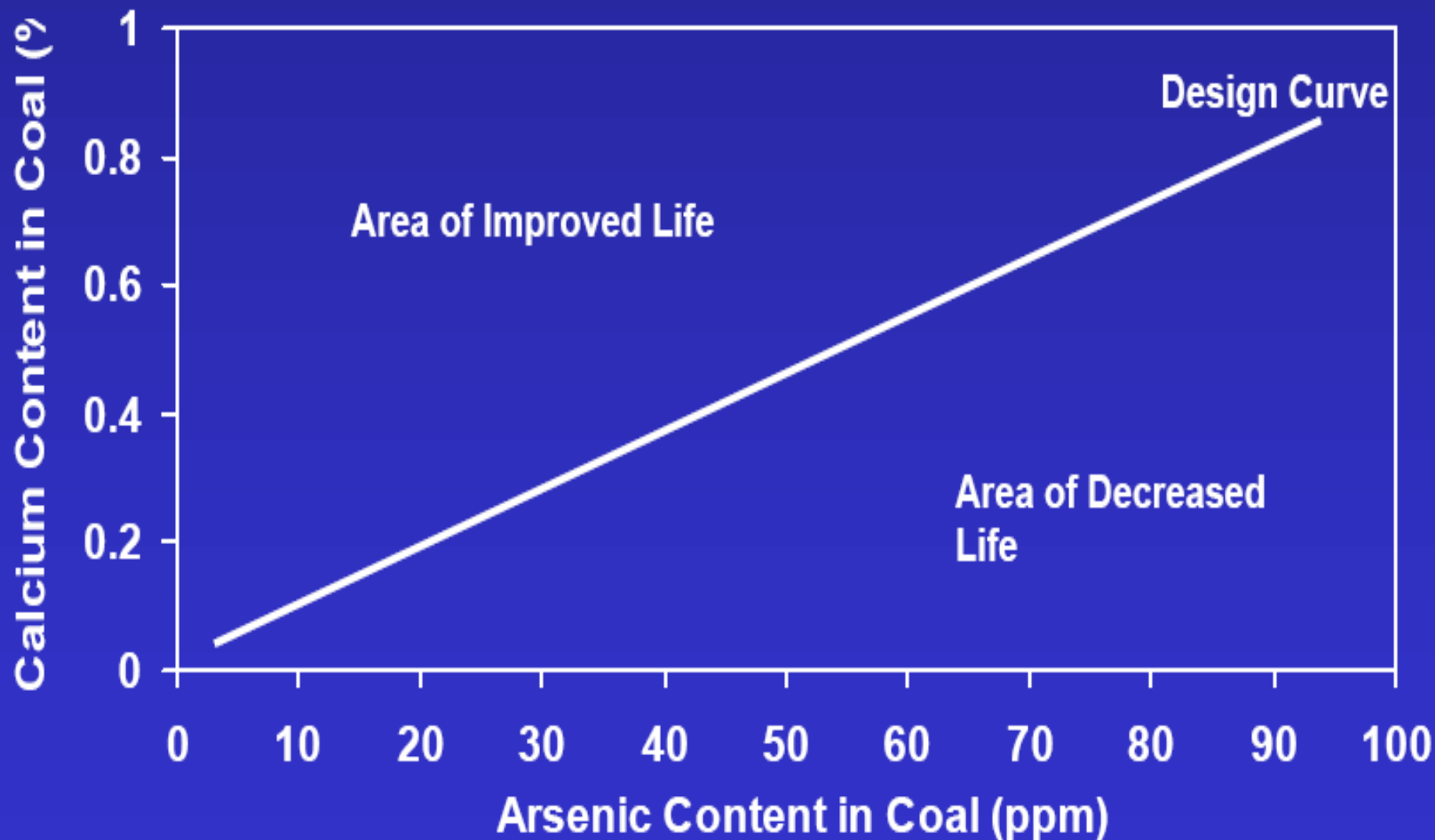
# Arsenic Poisoning



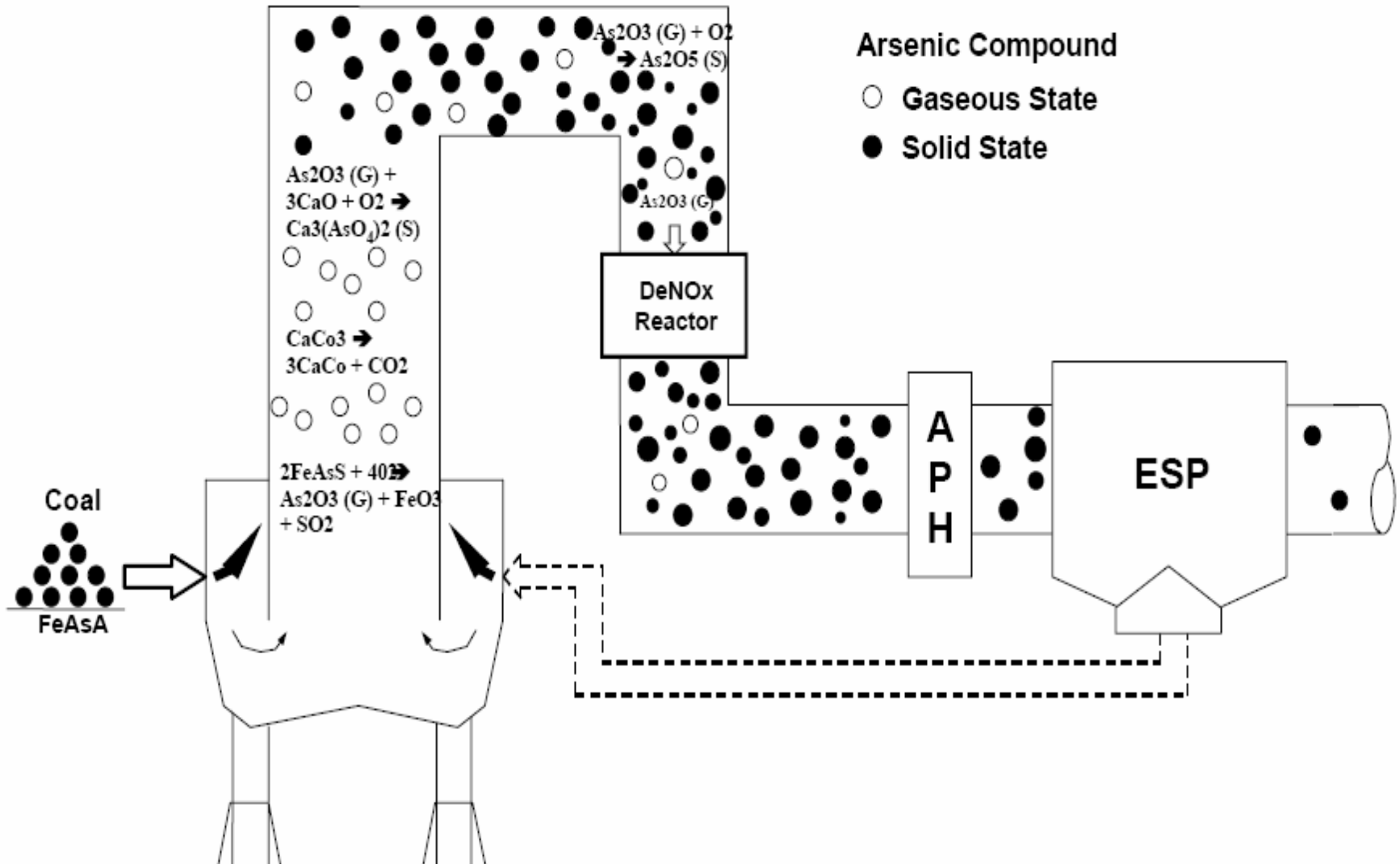
# Chemical Mechanism of Arsenic Poisoning



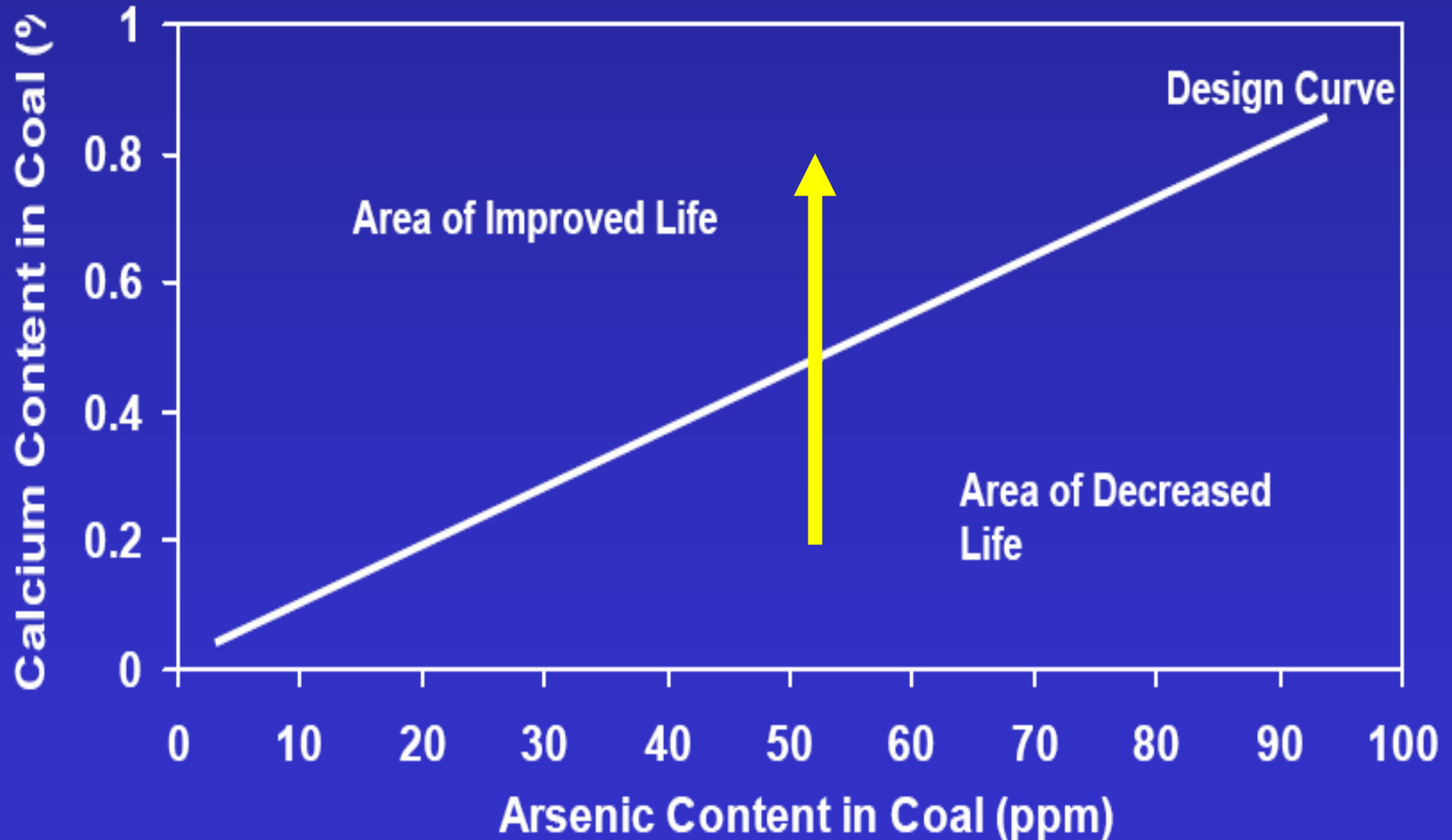
# Catalyst Life vs. Arsenic and Calcium in Fuel



# Limestone Injection



# Effect of Limestone Addition

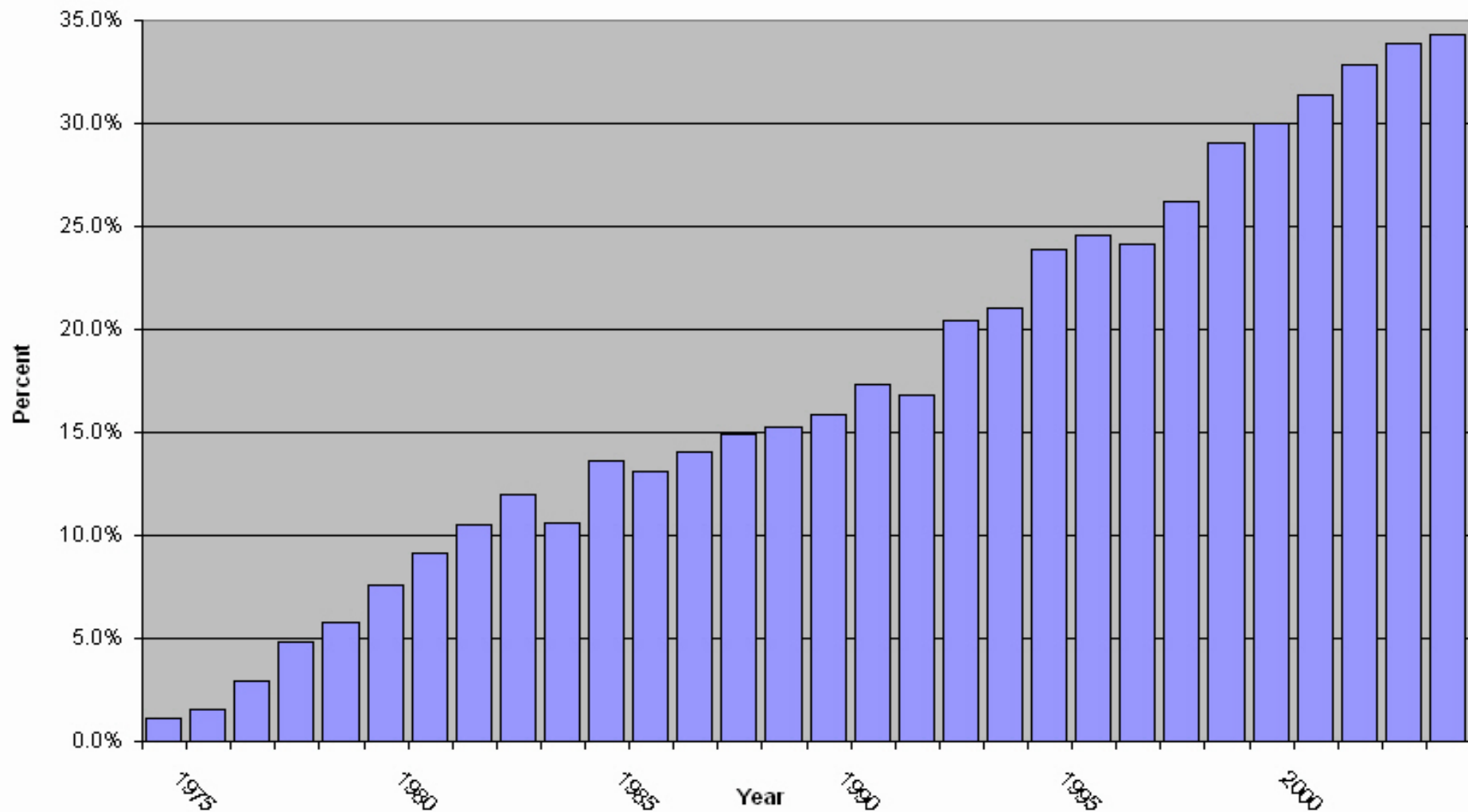


# PRB Coal



# PRB Coal Utilization

Percent of Total U.S. Coal Production Mined From The Powder River Basin, Wyoming



Sources: Energy Information Administration/Annual Energy Review, State Inspector of Mines of WY., & D.O.I. Federal Coal Management Report

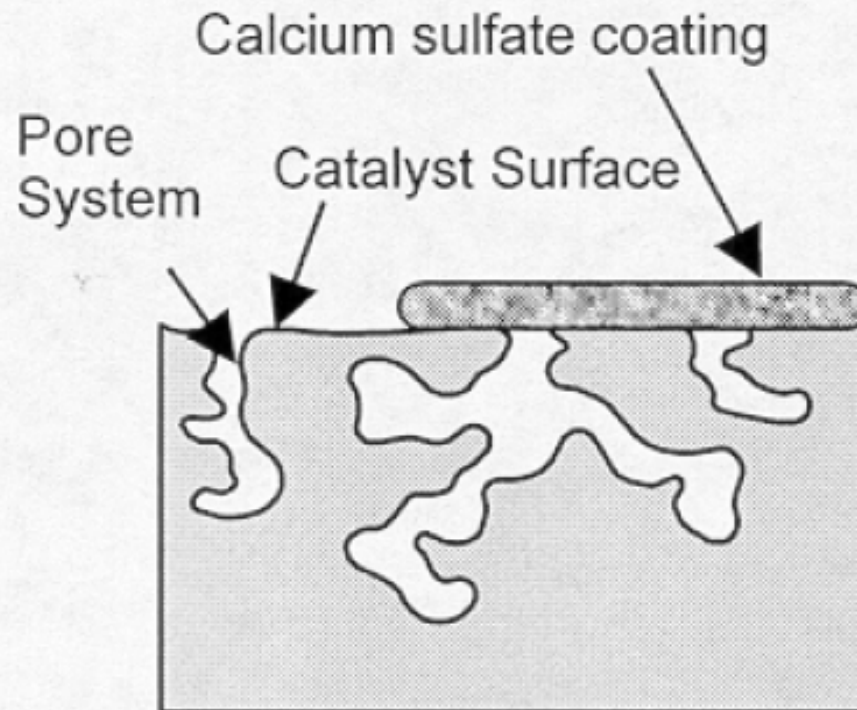
# PRB Coal

- Experience more recent than Bituminous, but still large
- **Poisoned by calcium (calcium sulfate)**
- Typically low sulfur levels, variable ash loading
- Sootblowing required
- Relaxed limits on  $\text{SO}_2$  conversion (sometimes)
- Effects on downstream equipment variable
- Ammonia slip typically  $< 2$  ppm, but not as critical as bituminous

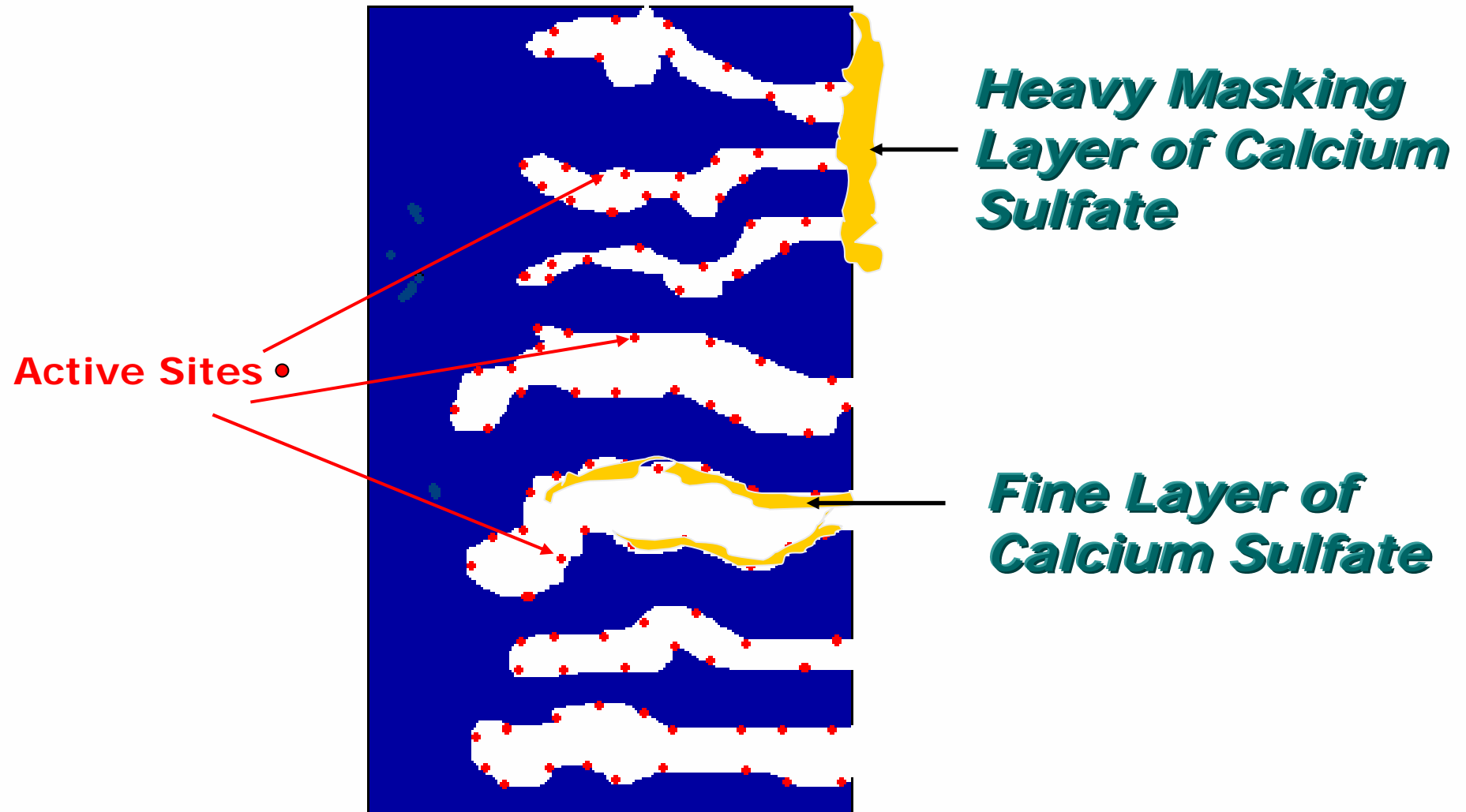
# Mechanism of PRB Poisoning

## PRB deactivation mechanism:

Macroscopic blockage of catalyst surface by calcium sulfate coating



# PRB Poisoning



# Mitigating PRB Poisoning

## ➤ Catalyst Design

➤ Good sootblowing, cleaning practices

➤ Good catalyst management plan

# Coal Blends

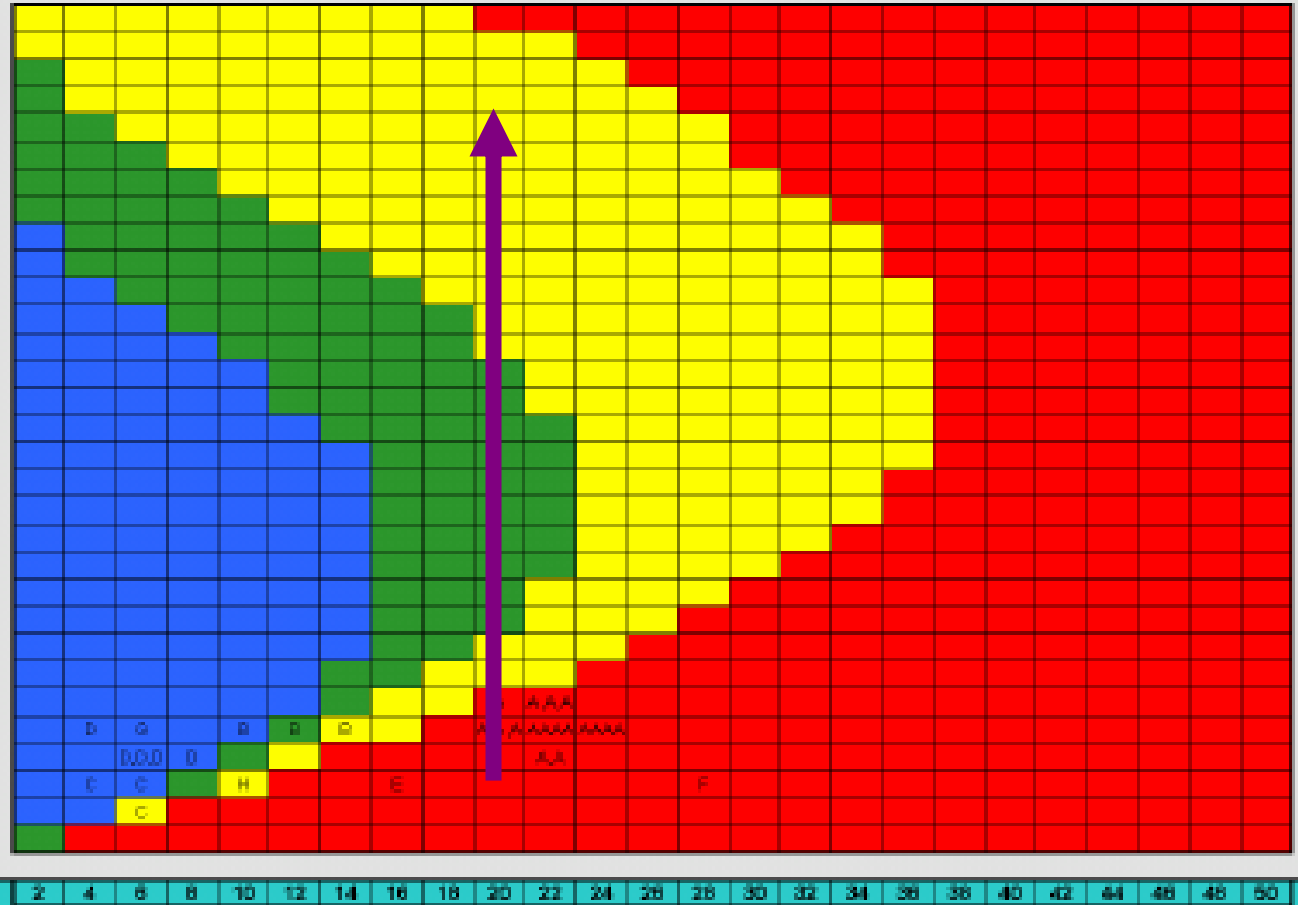
- Can have arsenic poisoning or calcium poisoning, depending on %
- Can produce wide range of flue gas/ash characteristics
- Can be used as poison mitigation

# Coal Blending Effect on Catalyst Life



Increasing PRB %

CaO in Fuel		CaO in 10% Ash		%
CaO in 15% Ash	CaO in 10% Ash	CaO in 10% Ash	CaO in 10% Ash	
10%	10%	10%	10%	
14.5	9.7	7.7	1.46	
14.1	9.4	7.4	1.41	
13.8	9.1	7.2	1.36	
13.1	8.7	6.9	1.31	
12.6	8.4	6.7	1.26	
12.2	8.1	6.4	1.22	
11.7	7.8	6.2	1.17	
11.2	7.5	5.9	1.12	
10.7	7.2	5.7	1.07	
10.3	6.8	5.4	1.03	
9.8	6.5	5.2	0.98	
9.3	6.2	4.9	0.93	
8.8	5.9	4.7	0.88	
8.4	5.6	4.4	0.84	
7.9	5.3	4.2	0.79	
7.4	4.9	3.9	0.74	
6.9	4.6	3.7	0.69	
6.5	4.3	3.4	0.65	
6.0	4.0	3.2	0.60	
5.5	3.7	2.9	0.55	
5.0	3.4	2.7	0.50	
4.6	3.0	2.4	0.46	
4.1	2.7	2.2	0.41	
3.6	2.4	1.9	0.36	
3.1	2.1	1.7	0.31	
2.7	1.8	1.4	0.27	
2.2	1.5	1.2	0.22	
1.7	1.1	0.9	0.17	
1.2	0.8	0.7	0.12	
0.8	0.6	0.4	0.08	
0.3	0.2	0.2	0.03	



CATALYST LIFE (Hours): X < 12,000 < X > 16,000 < X > 20,000 < X

# Guaranteed Catalyst Life

## Too Long

- Tied-up capital
- Can't take advantage of Catalyst Improvements
- Catalyst exposed needlessly to flue gas – deactivation
- Extra Pressure Drop

## Too Short

- Costly outages
- Logistics and purchasing costs

**QUESTIONS ?**